### DIOXIN REDUCTION BY SULFUR COMPONENT ADDITION

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#### 1. INTROCUCTION

Griffin has suggested that an addition of certain sulfur compounds to the fuel is effective for dioxin reduction<sup>1)</sup>. This study focused its attention to such sulfur addition and SO<sub>2</sub>, coal and pure sulfur were selected as sulfur sources.

#### 2. CONCEPTION

According to Griffin, the following 2 steps of reaction could be considered as one of formation process of dioxin<sup>1</sup>). That is,  $2HCl + 1/20_2 + Cl_2 + H_2O$  (1)  $Cl_2$  + aromatic compounds + chlorinated aromatic compounds (2) (partially dioxin)

HCl is oxidized by  $O_2$  and  $Cl_2$  is formed. (Reaction formula (1)). The reaction (1) is the so-called Deacon reaction and is known that the reaction proceeds with such transition metal compound as CuCl<sub>2</sub> as catalyst<sup>2</sup>). Since Cl<sub>2</sub> has high reactivity, it chlorinates the unburnt aromatic compounds in the combustor (reaction formula (2)). At this time, dioxin may be formed.

According to the above assumption, most effective procedure is to control the second reaction step. Therefore, a supply of sulfur to the combustor could be feasible. The sulfur content is converted into SO<sub>2</sub> and it reduces Cl<sub>2</sub> to HCl with the following reaction:  $SO_2 + Cl_2 + H_2O + SO_3 + 2HCl$  (3)

therefore, dioxin can be reduced.

ORGANOHALOGEN COMPOUNDS Vol. 19 (1994)

3. EXPERIMENT

Fig. 1 shows a flow sheet of fluidized bed combustor system used in this experiment. The test fluidized bed combustor is mainly composed by mullite of  $205 \text{mm}\phi \times 4\text{m}$ , and silica sand was used as a fluidizing medium.

In this experiment, gas components (HCl,  $SO_2$ , CO,  $CO_2$ ,  $O_2$ ) and inside temperature of the combustor, etc. were continuously measured. The mixture with the wood saw dust and PVC were fed to the combustor as a fuel. The wood saw dust contains lignin as the source of dioxin structure and PVC was expected as the source for chlorine. Sulfur was fed in the following modes within their molar ratio 0.075 to 3.8;

CASE A : Gaseous SO<sub>2</sub> was fed directly.

CASE B : Coal containing sulfur was fed.

CASE C : Coal and sulfur reagent were fed.

Our experimental conditions were shown in Table 1. The blank test in Table 1 meant the sulfur free condition and was used as our standard for comparing the other experimental conditions.



Fig. 1 Flow sheet of FBC test system

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The following incineration conditions were employed in this experiment;

O, (at exit flue gas) = 8%

② combustor temperature = 1000°C

3 fuel feed rate = 0.10~0.15 kg/min

Flue gas sampling method and dioxin analysis were completely along to the procedure established by the JAPAN WASTE RESEARCH FOUNDATION.

4. RESULTS AND DISCUSSION All data are summerized in Table 2.

4.1 Effects of gaseous SO<sub>2</sub> addition (CASE A) Fig. 2 shows that the more  $SO_2$  is fed, the less dioxin is formed. This result shows the reaction by formula (3) probably occurred and the results show that SO<sub>2</sub> in the abated gas is less than SO<sub>2</sub> in the unabated qas (Table 3). It also shows that the reaction defined by formula (3) occurred.

4.2 Effects of coal addition (CASE B) In this case, coal (containing sulfur) was added to the fuel. results are shown in Fig. 3. It indicates that an addition of coal greatly reduced an amount of dioxin. This means that gaseous SO, which was oxidized by O, in the combustor reduced dioxin by formula

(3). The reason for greater reduction effects by addition of coal than by addition of gaseous SO, is considered an active intermediate. It was generated in the combustor and worked on Cl, more actively than SO, did. But details remain unknown.

4.3 Effects of addition of coal+pure sulfur reagent (CASE C) All data including results of CASE C are plotted in Fig. 4. The results of CASE B show that an addition of coal was very effective. Therefore, in CASE C, pure sulfur reagent was further added to CASE B3 for much greater dioxin reduction. However, much greater effect for dioxin reduction could not be found, compared with CASE B. These data also show that the reduction effect varies depending on the mode of sulfur added into the fuel.

#### 5. CONCLUSION

Small scaled combustion tests were carried out with an addition of gaseous SO2, coal, pure sulfur reagent to the fuel, and the following conclusions are obtained: (1) Dioxin reduction occurs by gaseous  $SO_2$  addition to the fuel.

- (2) Dioxin reduction occurs by coal addition to the fuel and this effect is greater than the case of gaseous  $SO_2$  addition. It indicates that effect of dioxin reduction varies depending on the mode of sulfur addition.
- (3) Coal+pure sulfur reagent were added to the fuel for effect of dioxin reduction. However, further effect of dioxin reduction was not noted.

This combustion tests revealed that a presence of sulfur largely affect a reduction of dioxin. However, there are phenomena which can not yet be explained. Further basic studies are necessary for reduction of dioxin in the combustor.

#### REFERENCES

- 1) R.D. Griffin, Chemosphere, Vol. 15, Nos. 9-15, 1987(1986).
- Tadamitsu Kiyoura, Kenji Yoshida, Kiyoshi Shikai, Takayuki Mitani,

Yasuaki Totsuka, J. Chem. Soc. Jap., No. 9, 1672(1987).

		blank tast	SO₂ CASE A		coal CASE B			coal+S powder CASE C		
		DIANK LEST	A1	A2	A3	B1	B2	83	C1	C2
H₂O	*	15	15	15	15	8.3	8.5	8.4	8.5	8.5
0 <sub>2</sub>	X	8.0	8.3	8.0	8.0	8.3	8.1	8.4	8. 2	8.6
CO2	X	13	12	12	13	12	12	12	11	12
CO	×	50	44	39	80	150~450	100~400	120	100~350	100~400
SO2	ppm	0. 52	20	40	390	250	250	250	660	1050
NOx	ppm	72	68	70	66	220	250	250	290	260
HC l	ppm	1290	1360	1490	1310	1140	380	260	220	150
PCDDs	ng/Nm <sup>3</sup>	1400	1200	1000	470	14	15	6	15	3.5
PCDFs	ng/Nm³	5100	3300	2400	1300	27	18	7.6	24	5.6
total	ng/Nm³	6500	4500	3400	1800	41	33	14	39	9. 1

Table 1 Test conditions

Table 2 Test results

		blank test	CASE A			CASE B			CASE C	
			Al	A2	A3	B1	B2	B3	C1	C2
_ S/C1	mol/mol	0.075	0.17	0. 29	0.51	0.096	0.44	0.65	2.4	3.8
SO2	N1/min.	0	0. 16	0. 33	0.65	-	-	-	-	-
PVC	X	3. 3	3. 3	3.3	3.3	4.0	0.92	0. 57	0.56	0.56
coal	×	-	-	-	-	55	57	57	56	56
S Powder	X	-	-	-	-	-	-	-	0.68	1.3



Table 3 Sulfur balance (CASE A)

S	/01	0. 17	0. 29	0. 51		
Input	SO₂/ppm	310	530	950		
Output	SO₂/ppm	18	35	390		

Fig. 2 Influence of SO<sub>2</sub> gas



Fig. 3 Influence of coal

Fig. 4 Influence of sulfur

ORGANOHALOGEN COMPOUNDS Vol.19 (1994)